# PARAMOUNT TRANSMISSION LTD.

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NEB File 3400-P097-1 & 2620-D-4-7

June 24, 2002

National Energy Board 444 7th Avenue S.W. Calgary, Alberta T2P 0X8

Attention: Mr. Michel Mantha

Dear Sir;

Re: Paramount Transmission Ltd. Cameron Hills Pipeline and Fuel Gas Pipeline, Order XO-P097-02-2002 as amended; Conditions 14: Corrosion Inhibition Program

Paramount Transmission Ltd.'s (PTL) hereby submits three copies of the information requested in the National Energy Board's (NEB) letter of April 4, 2002 for its evaluation of PTL's corrosion inhibition program.

If further questions regarding the above matter then please contact the undersigned at (403) 290-3696 or by e-mail, tom.hong@paramountres.com.

Yours truly,

PARAMOUNT TRANSMISSION LTD.

Tom Hong, P.Eng.

Project Manager

Attachments

File Cameron Hills G 3.2

310460

# PARAMOUNT TRANSMISSION LTD. (PTL) CAMERON HILLS PIPELINE Order XO-P097-02-2002 as amended, Files 3400-P097-1 & 2620-D-4-7, Conditions 14: Corrosion Inhibition Program

Additional Information as requested in the National Energy Board (NEB) letter of April 4, 2002

# Request

- 1) data on:
  - a) the flow regime and water chemistry of the Bistcho Lake Area which is reportedly analogous to the Cameron Hills Pipeline; and
    - b) the water chemistry of the Cameron Hills Pipeline;
- 2) data and analysis on:
  - c) the similarities of the inhibitor programs of Bistcho Lake Area and the Cameron Hills Pipeline;

# Response

Table 1: Comparison between Bistcho Lake and Cameron Hills

	Bistcho Lake Area	Cameron Hills Pipeline
Flow Regime	The flow regime will vary depending on the gas and liquid production rates and the terrain (i.e. uphill or downhill) which the pipelines go through.	The terrain associated with the Cameron Hills Pipeline is generally sloping downhill slightly with some undulation in terrain when drainages or watercourses are encountered. The flow
	Generally, the flow regimes would be expected to be as follows:  Level terrain – Vary from mist to laminar  Uphill section – Slug flow  Downhill section – Laminar	regime is expected to be generally laminar.
Water Chemistry	25,000 to 70,000 ppm chlorides Two group stream water analyses from the Bistcho field are attached.	14,000 to 68,000 ppm chlorides Well and group stream water analyses from the Cameron Hills field are attached.
Similarities of the Proposed Inhibitor Programs:		
Batch Chemical	Techni-Hib 3169 based on a 1 mil film thickness.	Techni-Hib 3169 based on a 1 mil film thickness.
Continuous Injection Chemical	RCI-00125 based on 200 ppm in liquid phase	RCI-00125 based on 200 ppm in liquid phase

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# PARAMOUNT TRANSMISSION LTD. (PTL) CAMERON HILLS PIPELINE Order XO-P097-02-2002 as amended, Files 3400-P097-1 & 2620-D-4-7, Conditions 14: Corrosion Inhibition Program

Additional Information as requested in the National Energy Board (NEB) letter of April 4, 2002

#### Table 1 - continued

	Bistcho Lake Area	Cameron Hills Pipeline
	·	
Corrosion Coupon Monitoring	Every 90 days	Every 90 days
Iron & Manganese – Field	Every 2 months	Every 2 months
Iron & Manganese - Plant	Monthly	Monthly
Corrosion rate calculations	Monthly	Monthly
SRB <sub>(1)</sub> Analysis – Field	Quarterly	Quarterly
SRB Analysis – Plant	Monthly	Monthly
APB <sub>(2)</sub> Analysis – Field	Quarterly	Quarterly
APB Analysis - Plant	Monthly	Monthly
Full Scale Analysis	Every 6 months	Every 6 months
Millipore Gas Sampling	Quarterly	Quarterly
Notes:	Actual frequencies may vary depending	Actual frequencies may vary depending
(1) Sulphide reducing bacteria (2) Acid producing bacteria	on the scheduling of activities and the trending of the data.	on scheduling of the activities and the trending of the data.

# Request

- 2) data and analysis on:
  - d) the effect of methanol on the corrosion inhibitor film specific to the Cameron Hills Pipeline;

#### Response

The two influences of methanol on the corrosion inhibition film are as follows:

- The liquid volume added to the pipeline; and
- The addition of oxygen to system.

Results from experiments performed by BJ Services Company Ltd, who is implementing the corrosion inhibition program for PTL, show that oxygen-free methanol at 5-12% by volume in a brine solution does not accelerate uninhibited corrosion. However, oxygen added to a system with  $H_2S$  and  $CO_2$  increased the uninhibited corrosion rate by as much as a factor of ten depending on the amount of oxygen added.

The specific inhibitors used in the Bistcho Lake Field and Cameron Hills have been laboratory tested for their tolerance to methanol. The inhibitor effectiveness, expressed by the equation: (uninhibited corrosion rate – inhibited corrosion rate)/ uninhibited corrosion rate, decreased by only 0.4% for the oil soluble inhibitor and 0.8% for the water soluble inhibitor in the presence of

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# PARAMOUNT TRANSMISSION LTD. (PTL) CAMERON HILLS PIPELINE Order XO-P097-02-2002 as amended, Files 3400-P097-1 & 2620-D-4-7, Conditions 14: Corrosion Inhibition Program

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5% methanol. This is a negligible influence which is less than the limits of experimental accuracy.

## Request

- 2) data and analysis on:
  - e) the effect of water chemistry on the corrosion inhibitor water dispersibility for the Cameron Hills Pipeline.

# Response

The RCI-00125 inhibitor is soluble in the range of water chemistry at Cameron Hills. The Techni-Hib 3169 inhibitor has limited dispersibility in the range of water chemistry at Cameron Hills.

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Company:	Parmount Res. Ltd.
NRD#	02-013
Sample #	P-8546N

LSD	North Inlet
Date D/M/Y	Jan22/2002

Cations			
lon	mg/L	mmoles/L	,meq/L
Na	35100	1526.8	1526.8
K	1010	25.8	25.8
Ca	7290	181.9	363.8
Mg	1850	76.1	152.2
Fe	<0,01	0.0	0.0
Ba	0.27	0.00	0.00
Sr	339	3.87	7.74
otal	45589.27	1814.5	2076.3

Anions			
Ion	mg/L	mmoles/L	meq/L
CI	63400	1788.3	1788.3
SO4 .	1050	10.9	21.9
HCO3	752	12.3	12.3
CO3	ND	0.0	0.0
ОН	ND	0.0	0,0
		`	
Total	65202	1811.5	1822.5

Ionic Strength 4	2.214
pH (@ 22 °C)	6,77
Bottom Hole Temperature ( ° C)	4(
K-factor at 40 ° C	3
H2S Present:	Ye:
	25.0000 million 1000 million 1000 0000

Total Hardness (mg/L as CaCO3) 25818
Total Alkalinity (mg/L as CaCO3) 617
Calculated Dissolved Solids (mg/L) 110791
Specific Gravity (@ 15.6°C) 1.0751
Specific Gravity (as mg/L NaCl) 105841

#### CaCO3 Scaling Index Calculations

Stability Index at 40 ° C

1.12

St > 0, so CaCO3 Scale is likely to form.

#### **CaSO4 Scaling Prediction**

CaSO4 Ksp at 40 ° C 29£0 Solubility Limit meq/L 30.9

Actual CaSO4 Conc. in meq/L 21.9

Limit > Actual, so CaSO4 Scale is unlikely to form

#### **BaSO4 Scaling Prediction**

BaSO4 Ksp at 40 ° C

Solubility Limit meq/L

Actual BaSO4 Conc. in meq/L

0.0039

Limit - Actual so BaSO4 Scale is unlikely to form

#### **SrSO4 Scaling Prediction**

SrSO4 Ksp at 40 ° C
Solubility Limit meq/L
Actual SrSO4 Conc. in meq/L
7.7

Limit < Actual, so 5r5O4 Scale is likely to form:



Company:	Parmount Res. Ltd.
NRD#	02-013
Sample #	P-8546D

1 011200	The second secon
LSD	South Inlet
Date D/M/Y	Jan22/2002

Cations				
lon	mg/L	mmoles/L	meq/L	
Na	21900	952.6	952.6	
К	432	11.0	11.0	
Ca	3680	91.8	183.6	
Mg	1980	81.5	162.9	
Fe	0.16	0.0	0.0	
Ва	84.6	0.62	1.23	
Sr	540	6.16	12.33	
Total	28616.76	1143.7	1323.8	

Anions			
lon.	mg/L	mmoles/L	meq/L
CI	52300	1475.2	1475.2
SO4	44	0.5	0.9
нсоз	811	13.3	13.3
CO3	ND	0.0	0.0
ОН	ND	0.0	0.0
i i			
Total	53155	1488.9	1489.4

Ionic Strength μ pH (@ 22 °C) Bottom Hole Temperature (°C)	1.578 6.82
K-factor at 40 ° C H2S Present:	3.15 Yes

Total Hardness (mg/L as CaCO3) 17493
Total Alkalinity (mg/L as CaCO3) 665
Calculated Dissolved Solids (mg/L) 81772
Specific Gravity (@ 15.6°C) 1.0532
Specific Gravity (as mg/L NaCl) 74977

#### **CaCO3 Scaling Index Calculations**

Stability Index at 40 ° C

0.76

St > 0, so CaCO3 Scale is likely to form

#### **CaSO4 Scaling Prediction**

CaSO4 Ksp at 40 ° C

2.5E-03

Solubility Limit meq/L

43.5

Actual CaSO4 Conc. in meq/L

0.9

Limit > Actual, so CaSO4 Scale is unlikely to form

# **BaSO4 Scaling Prediction**

BaSO4 Ksp at 40 ° C

1.8E-08

Solubility Limit meg/L

0.1533

Actual BaSO4 Conc. in meq/L

0.9162

Limit < Actual, so BaSO4 Scale is likely to form.

#### **SrSO4 Scaling Prediction**

SrSO4 Ksp at 40 ° C

1.8E-05

Solubility Limit meq/L

4.5

Actual SrSO4 Conc. in meq/L

0.9

Limit > Actual, so SrSO4 Scale is unlikely to form



Company:	Paramount Resources Ltd.
NRD#	02-396
Sample #	P.ROSOC

LSD	Well A-73
Date D/M/Y	May 15/2002

Cations			
lon	mg/L	mmoles/L	meq/L
Na	1771	77.0	77.0
Κ	113	2.9	2.9
Ca	1725	43.0	86.1
Mg	730	30.0	60.1
Fe	0.05	0.0	0.0
Ba	0.29	0.00	0.00
Sr	6.15	0.07	0.14
Total	4345.49	153.1	226.2

Anions			
lon	mg/L	mmoles/L	meq/L
CI	7600	214.4	214.4
SO4	190	2.0	4.0
HCO3	242	4.0	4.0
CO3	ND	0.0	0.0
ОН	ND	0.0	0.0
Total	8032	220.3	222.3

Ionic Strength μ	0.299
pH (@ 22 °C)	6.87
Bottom Hole Temperature ( ° C)	40
K-factor at 40 ° C	2.65
H2S Present:	No
	>1000000000000000000000000000000000000

Total Hardness (mg/L as CaCO3) 7313
Total Alkalinity (mg/L as CaCO3) 198
Calculated Dissolved Solids (mg/L) 12377
Specific Gravity (@ 15.6°C) 1.0065
Specific Gravity (as mg/L NaCl) 9161

#### **CaCO3 Scaling Index Calculations**

Stability Index at 40 ° C

0.45

SI > 0, so CaCO3 Scale is likely to form

# **CaSO4 Scaling Prediction**

CaSO4 Ksp at 40 ° C

6.8E-04

Solubility Limit meq/L

25.3

Actual CaSO4 Conc. in meg/L

25.3 4.0

Limit > Actual, so CaSO4 Scale is unlikely to form

#### **BaSO4 Scaling Prediction**

BaSO4 Ksp at 40 ° C

5.0E+09

Solubility Limit meq/L

0.0051

Actual BaSO4 Conc. in meq/L

0.0031

Limit > Actual, so BaSO4 Scale is unlikely to form

#### SrSO4 Scaling Prediction

SrSO4 Ksp at 40 ° C

4.0E-06

Solubility Limit meq/L

2.5

Actual SrSO4 Conc. in meq/L

2.0

Limit × Actual, so SrSO4 Scale is unlikely to form



Company:	Paramount Resources Ltd.
NRD#	02-396
Sample #	P-8930A

LSD	Well B-08
Date D/M/Y	May 15/2002

	C	ations	
lon	mg/L	mmoles/L	meq/L
Na	24500	1065.7	1065.7
K	2440	62.4	62.4
Ca	13600	339.3	678.6
Mg	2190	90.1	180.2
Fe	0.83	0.0	0.0
Ba	0.53	0.00	0.01
Sr	120	1.37	2.74
Total	42851.36	1558.9	1989.7

Anions			
lon	mg/L	mmoles/L	meq/L
CI	67200	1895.5	1895.5
SO4	925	9.6	19.3
HCO3	114	1.9	1.9
CO3	NĐ	0.0	0.0
ОН	ND	0.0	0.0
Total	68239	1907.0	1916.6

lonic Strength μ pH (@ 22 °C) Bottom Hole Temperature ( ° C) K-factor at 40 ° C H2S Present:	2.391 6.78 40 2.95 No
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Total Hardness (mg/L as CaCO3) 42976
Total Alkalinity (mg/L as CaCO3) 93
Calculated Dissolved Solids (mg/L) 111090
Specific Gravity (@ 15.6°C) 1.0797
Specific Gravity (as mg/L NaCl) 112324

### **CaCO3 Scaling Index Calculations**

Stability Index at 40 ° C

0.63

St ≥ 0, so CaCO3 Scale is likely to form

### **CaSO4 Scaling Prediction**

CaSO4 Ksp at 40 ° C
Solubility Limit meq/L
Actual CaSO4 Conc. in meq/L
17.5
19.3

Limit \* Actual, so GaSO4 Scale is likely to form

# **BaSO4 Scaling Prediction**

BaSO4 Ksp at 40 ° C

Solubility Limit meq/L

Actual BaSO4 Conc. in meq/L

0.0077

Umit < Actual, so BaSOA Scale is likely to form

# SrSO4 Scaling Prediction

SrSO4 Ksp at 40 ° C

Solubility Limit meq/L

Actual SrSO4 Conc. in meq/L

2.7

Limit < Actual, so StSO4 Scale is likely to form



Company:	Paramount Resources Ltd.	LSD	Well C-50
NRD#	02-396	Date D/M/Y	May 15/2002
Sample #	P_8930B		

Cations			
ion	mg/L	mmoles/L	meq/L
Na	261	11.4	11.4
K	19.8	0.5	0.5
Ca	181	4.5	9.0
Mg	26.4	1.1	2.2
Fe	0.27	0.0	0.0
Ba	0.05	0.00	0.00
Sr	2.43	0.03	0.06
otal	490.95	17.5	23.1

lon	mg/L	mmoles/L	meq/L
1011	mg/E	IIII/Oles/L	meqr
CI	660	18.6	18.6
SO4	250	2.6	5.2
HCO3	145	2.4	2.4
CO3	ND	0.0	0.0
ОН	ND	0.0	0.0
Total	1055	23.6	26.2

lonic Strength μ	0.033	Total Hardness (mg/L as CaCO3)	561
pH (@ 22 °C)	7.5	Total Alkalinity (mg/L as CaCO3)	119
Bottom Hole Temperature ( ° C)	40	Calculated Dissolved Solids (mg/L)	1546
K-factor at 40 ° C	1.9	Specific Gravity (@ 15.6°C)	1.0045
H2S Present:	No	Specific Gravity (as mg/L NaCl)	6342

#### **CaCO3 Scaling Index Calculations**

Stability Index at 40 ° C

0:63

St > 0, so CaCO3 Scale is likely to form.

#### **CaSO4 Scaling Prediction**

CaSO4 Ksp at 40 ° C 2.0E-04 Solubility Limit meq/L 26.4

Actual CaSO4 Conc. in meg/L 5.2

Limit > Actual, so CaSO4 Scale is unlikely to form

#### **BaSO4 Scaling Prediction**

BaSO4 Ksp at 40 ° C 1.0E-09 Solubility Limit meg/L 0.0008 Actual BaSO4 Conc. in meq/L 0.0007

#### SrSO4 Scaling Prediction

SrSO4 Ksp at 40 ° C Solubility Limit meq/L 0.2 Actual SrSO4 Conc. in meq/L 0.1

Limit of Actual, so SrSO4. Scale is unlikely to form



# CAMERON PIPELINE WATER ANALYSIS

(INCLUDES SOME BISTCHO WELLS)

# WATER ANALYSIS AND

# SCALING TENDENCY CALCULATIONS

Company:	Paramount Resources Ltd.	LSD	12" Line @ Bistcho Lake
NRD#	02-396	Date D/M/Y	May 15/2002
Sample #	P-8930D		3.334.334.334.334.334.334.334.334.334.3

Cations			
lon	mg/L	mmoles/L	meq/L
Na	2620	114.0	114.0
K	11200	286.5	286.5
Ca	4520	112.8	225.5
Mg	726	29.9	59.7
Fe	0.25	0.0	0.0
Ва	1.18	0.01	0.02
Sr	31	0.35	0.71
Total	19098.43	543.4	686.4

lon	mg/L	mmoles/L	meq/L
CI	24600	693.9	693.9
SO4	1200	12.5	25.0
нсоз	631	10.3	10.3
CO3	89.7	1.5	2.9
ОН	ND	0.0	0.0
Total	26520.7	718.2	732.1

Ionic Strength μ	0.866	Total Hardness (mg/L as CaCO3)	14277
pH (@ 22 °C)	8.4	Total Alkalinity (mg/L as CaCO3)	667
Bottom Hole Temperature ( ° C)	40	Calculated Dissolved Solids (mg/L)	45619
K-factor at 40 ° C	3.05	Specific Gravity (@ 15.6°C)	1.0177
H2S Present:	No	Specific Gravity (as mg/L NaCl)	24945

# **CaCO3 Scaling Index Calculations**

Stability Index at 40 ° C

2.48

St > 0, so CaCC3 Scale is likely to form

# CaSO4 Scaling Prediction

CaSO4 Ksp at 40 ° C	2.2E-03	
Solubility Limit meq/L	37.6	
Actual CaSO4 Conc. in meg/L	25.0	

Limit > Actual, so CaSO4 Scale is unlikely to form

#### **BaSO4 Scaling Prediction**

BaSO4 Ksp at 40 ° C	1.1E-08	
Solubility Limit meq/L	0.0018	
Actual RaSO4 Conc. in med/l	0.0172	

Limit < Artholish BaSO4 Scale is likely to form.

# SrSO4 Scaling Prediction

SrSO4 Ksp at 40 ° C	1.1E-05
Solubility Limit meq/L	1.8
Actual SrSO4 Conc. in meg/L	0.7

Limit > Actual, so SrSO4 Scale is unlikely to form.